Seat No.:	Enrolment No.

## GUJARAT TECHNOLOGICAL UNIVERSITY BE - SEMESTER- IV(NEW) EXAMINATION - SUMMER 2015

Subject Code: 2140503 Date:03/06/2015

Subject Name: Process Heat Transfer

Time: 10:30am-1.00pm Total Marks: 70

**Instructions:** 

- 1. Attempt all questions.
- 2. Make suitable assumptions wherever necessary.
- 3. Figures to the right indicate full marks.
- Q.1 (a) Derive equation for heat transfer through a composite wall made up of 3 different materials in close thermal contact with each other, with no heat loss to surrounding when temperatures of hot and cold ends are  $T_h$  and  $T_c$ .
  - (b) A flat surface wall is constructed of a 115 mm layer of sil-o –cell brick with a thermal conductivity 0.4651 watt/m c backed by a 230 mm layer of common brick with thermal conductivity4.651watt/m c. The temperature of inner surface of the wall is 760° C and that of outer surface is 77° C. (i) What is the heat loss through the wall in Kw? (ii) What is temperature of the interface between the refractory brick and common brick?
- Q.2 (a) Draw the temperature profiles of cold and hot fluids for true co-current and counter –current flow in double pipe heat exchanger, Derive expression relating Rate of heat transfer and Log mean temperature difference.
  - (b) Water flowing at the rate 0.15 kg/sec is heated from 40° C to 80°C in a counter flow double pipe heat exchanger. The hot fluid is oil and enters exchanger at 105 °C and leaves at 70° C. Calculate heat transfer area if overall heat transfer coefficient is 300 w/m² °C. Sp. heat of water is 4.186 kj/kg °C.

OR

- (b) Discuss Natural convection. Show the velocity and temperature profile for natural convection from heated vertical plate.
- Q.3 (a) With the help of Diagram of 1-2 Shell & Tube heat exchanger explain function of various parts of exchanger.
  - (b) Methyl Alcohol flowing in the inner pipe of a double pipe exchanger is cooled with water flowing in the jacket. The ID and OD of inner pipe are 25 and 32 mm respectively. The thermal conductivity of Steel is 45 W/m C. The individual coefficient and fouling factors are as under.

Alcohol Co-eeficient ,  $h_i$  1020 W/m<sup>2</sup> C WaterCo-eeficient ,  $h_o$  1700 W/m<sup>2</sup> C

Inner Fouling factor, h<sub>di</sub> 5680 W/m<sup>2</sup> C Outer Fouling factor, h<sub>do</sub> 5680 W/m<sup>2</sup> C

What is overall heat transfer coefficient based on outside area of inner pipe?

OR

- Q.3 (a) Using Dimension analysis derive expression for forced convection for the fluid flowing inside tube in a turbulent flow.
  - (b) With the neat diagram show various ways to provide extended surface in an exchanger.
- Q.4 (a) State laws of radiation. Explain Black body.

(b) Determine the net radient interchange between two parallel oxidized iron plates at a distance of 25 mm, having side of  $3m \times 3m$ . The surface temperature of the two plates are 100 C and 40 C respectively. Emmissivities of the plates are 0.736.

## OR

- Q.4 (a) Show different type of feeding arrangement for triple effect evaporator with 07 advantages and disadvantage.
  - (b) An evaporator is to be fed with 5000 Kg/hr of 10 % sugar solution by weight. The feed at 40°C is to be concentrated to a solution containing 40 % by wt of solute under an absolute pressure of 1.03 kg/cm². Steam is available at an absolute pressure of 3atm (Saturation temp of 134°C). The overall heat transfer coefficient is 1750 w/m² C. Calculate heat transfer area required and the steam requirement.
- Q.5 (a) Discuss with the help of diagram various regimes of pool boiling. What is the use of finding critical flux and critical temperature drop?
  - **(b)** Discuss condensation on Vetical surface.

## OR

- Q.5 (a) Discuss construction and working of Plate type heat exchanger.
  - (b) Discuss LMTD correction factor. 07

Data for Q.4(b) (OR)

Temperature, °C	Enthalp	y.kj./kg
	Vapor	Liquid
40	2568	169.5
100	2675.7	418.6
134	2726.75	562.6

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