

**GUJARAT TECHNOLOGICAL UNIVERSITY****ME - SEMESTER– I (New course)• REMEDIAL EXAMINATION – SUMMER 2015****Subject Code: 2711101****Date:13/05/2015****Subject Name: Advanced Thermodynamics & Heat Transfer****Time: 10:30 am to 1:00 pm****Total Marks: 70****Instructions:**

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.

**Q.1 (a)** What are the mechanisms of heat transfer? How are they distinguished from each other? **07**

**(b)** Explain in brief the increase of entropy principle **07**

**Q.2 (a)** Derive an expression for the availability of a closed system. **07**

**(b)** 5 kg of air at 550K and 4 bar is enclosed in a closed system. Determine the availability of the system if the surrounding pressure and temperature are 1 bar and 290K respectively. **07**

**OR**

**(b)** A heat source at 800 K loses 2000 kJ of heat to a sink at (a) 500 K and (b) 750 K. Determine which heat transfer process is more irreversible. **07**

**Q.3 (a)** Derive the general heat conduction equation for Cartesian Co-ordinates **07**

**(b)** A carbon steel rod ( $k = 55 \text{ W/m}^\circ\text{C}$ ) has been attached to a plane wall which is maintained at a temperature of  $350^\circ\text{C}$ . The rod is 8 cm long and has cross section of an equilateral triangle with each side 5 mm. Determine the heat dissipation from the rod if it is exposed to a convection environment at  $25^\circ\text{C}$  with value of  $h = 100 \text{ W/m}^2\text{C}$ . Consider end surface loss to be negligible. **07**

**OR**

**Q.3 (a)** Prove that the temperature of a body at any time  $\tau$  during Newtonian heating or cooling is given by the relation **07**

$$\frac{t - t_a}{t_i - t_a} = \exp [-B_i F_o],$$

Where  $B_i$  and  $F_o$  are the Biot and Fourier modulus respectively;  $t_a$  is ambient temperature and  $t_i$  is the initial temperature of the body.

**(b)** Discuss the numerical formulation and solution of two-dimensional steady heat conduction in rectangular coordinates using the finite difference method. **07**

**Q.4 (a)** What do you understand by the hydrodynamic and thermal boundary layers? Illustrate with reference to flow over a flat heated plate. **07**

**(b)** Engine oil at  $60^\circ\text{C}$  flows over the upper surface of a 5-m-long flat plate whose temperature is  $20^\circ\text{C}$  with a velocity of 2 m/s. Determine the total drag force and the rate of heat transfer per unit width of the entire plate. The properties of engine oil at the film temperature of  $T_f = 40^\circ\text{C}$  are  $\rho = 876 \text{ kg/m}^3$ ,  $\text{Pr} = 2870$ ,  $k = 0.144 \text{ W/m}^\circ\text{C}$ ,  $\nu = 242 \times 10^{-6} \text{ m}^2/\text{s}$  **07**

**Q.4 (a)** What is natural convection? How does it differ from forced convection? What force causes natural convection currents? **07**

**(b)** Hot air at atmospheric pressure and  $80^\circ\text{C}$  enters an 8m-long uninsulated square duct of cross section  $0.2 \text{ m} \times 0.2 \text{ m}$  that passes through the attic of a house at a rate of  $0.15 \text{ m}^3/\text{s}$ . The duct is observed to be nearly isothermal at  $60^\circ\text{C}$ . Determine the exit temperature of the air and the rate of heat loss from the duct to the attic space. Use following properties of air for the calculation. **07**

$\rho = 0.9994 \text{ kg/m}^3$ ,  $C_p = 1008 \text{ J/kgK}$ ,  $\mu = 910 \times 10^{-6}$ ,  $k = 0.02953 \text{ W/mK}$ ,  $\text{Pr} = 0.7154$ ,  $\nu = 2.097 \times 10^{-5} \text{ m}^2/\text{s}$ .

- Q.5 (a)** Explain Kirchhoff's law. What do you mean by the statement: A perfect absorber of radiant energy is also a perfect emitter? **07**
- (b)** How does the Nusselt's equation for condensation on a horizontal tube differ from that on a vertical tube? **07**
- Q.5 (a)** Draw the boiling curve and identify the burnout point on the curve. Explain how burnout is caused. Why is the burnout point avoided in the design of boilers? **07**
- (b)** Explain how Hottel's curves can help in estimating radiant heat exchange between a gas volume and an enclosure. **07**

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