GUJARAT TECHNOLOGICAL UNIVERSITY

ME - SEMESTER- I (New course)• REMEDIAL EXAMINATION – SUMMER 2015 Subject Code: 2711601 Date:13/05/2015

Subject Name: Advanced Thermodynamics

Time: 10:30 am to 1:00 pm

Instructions:

- 1. Attempt all questions.
- 2. Make suitable assumptions wherever necessary.
- 3. Figures to the right indicate full marks.
- Q-(1) (a) Write briefly about criteria of chemical reaction equilibria and standard (06) conditions. Hence or otherwise, discuss about ranges of the following:-
 - (i) ΔG : Free Energy Change for reaction under actual conditions.
 - (ii) ΔG° : Free Energy Change for reaction under standard conditions.
 - (iii) K : Equilibrium constant for chemical reaction equilibria.
 - (iv) x_e : Equilibrium constant for reaction under actual conditions.

Production methanol proceeds as follows:-

(08)

Total Marks: 70

(b)

$CO + 2H_2 \rightarrow CH_3OH.$

The reaction under consideration is carried out at temperature (t) = 390 °C and pressure (p) = 300 atm. The value of ratio α of activity coefficients (Kr) is 0.434 and the value of free energy change for reaction at 663.2 °K is + 14,700 Cal/gmole. Show that the values of yield of methanol and equilibrium conversion are 21% and 45% respectively.

- Q-(2) (a) Starting from first principals, derive an expression for Heat of Reaction for a (07) reaction of type $a \cdot A + b \cdot B \Leftrightarrow c \cdot C + d \cdot D$ occurring at any temperature (T) and any pressure (p) under non-ideal conditions. Describe with the help of appropriate data & equations and relevant graphs, (07)
- (b) the calculation of equilibrium conversion under adiabatic conditions for a reaction of type $A \rightarrow B$ being highly reversible and exothermic in nature.

OR

- (b) Describe with the help of appropriate data & equations and relevant graphs, (07) the calculation of equilibrium conversion under adiabatic conditions for a reaction of type $A \rightarrow B$ being highly reversible and endothermic in nature.
- Q-(3) (a) Explain calculations of equilibrium conversion values under isothermal (07) conditions for the following two reactions proceeding simultaneously: A→B+C & A→D+E. Derive relevant equations for equilibrium constant (K) as a function of P, nt & xe. Also briefly decribe stepwise procedure for calculation of values of xe when both reactions proceed simultaneously.
 - (a) Describe with the help of appropriate data & equations and relevant graphs, (07) the calculation of equilibrium conversion under non-isothermal & non-adiabatic conditions for a reaction of type A→B being highly reversible and exothermic or endothermic in nature.

- (b) Explain the adiabatic flash calculations with block diagram and supporting (07) equations
- Q4

For 200 kW (56.87 TR) ammonia water absorption refrigeration plant (14) determine the followings.

- a. Flow rate of ammonia required in cycle. Consider 2.5 % heat gain.
- b. Calculate the heat duty of absorber. Heat of solution of ammonia= $2000 \text{ kJ/kg of NH}_3$
- c. Calculate the heat duty of condenser of distillation column. Reflux ratio of distillation column is 0.3137.Condensation temperature of ammonia vapour in condenser = $40 \,^{\circ}$ C.
- d. Calculate the heat duty of generator (reboiler) of distillation column.e. Calculate the COP.

DATA:

Temprature, ^o C	Saturation Pressure,kP	$H_{L,}$ kJ/kg	$H_{V_{i}}$ kJ/kg
	а		
-10	290.75	301.4	1597.8
40	1555.5	538.5	1637.2

OR

- Q4 (a) Explain with neat sketch the working of Lithium Bromide water Vapour (07) absorption refrigeration cycle.
 - (b) Explain with neat sketch the working of modified Vapour Compression (07) refrigeration cycle.
- Q5 (a) Explain method for DEWT calculation with the help of block diagram and (07) all supportive equations.
 - (b) With Txy and Pxy diagram discuss vapor-liquid-liquid equillibrium. (07)

OR

- Q5 (a) Explain method for DEWP calculation with the help of block diagram and (07) all supportive equations.
 - (b) Explain method for BUBLP calculation with the help of block diagram (07) and all supportive equations.