

Seat No.: _____

Enrolment No. _____

GUJARAT TECHNOLOGICAL UNIVERSITY**M.E –IIst SEMESTER–EXAMINATION – JULY- 2012****Subject code: 1723903****Date: 10/07/2012****Subject Name: Thermal Equipment Design****Time: 10:30 am – 13:00 pm****Total Marks: 70****Instructions:**

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.
4. Use of Steam table and Refrigeration table are permitted.

- Q.1** (a) Explain step by step the methodology for design of heat exchanger. **07**
 (b) Steam condenses at atm. pressure on the external surface of tubes of the steam condenser. **07**
 The tubes are 12 in nos. and each is 30 mm in diameter and 10mm long. The inlet and outlet temp. of cooling water flowing inside the tubes are 25°C and 60°C resp. If the flow rate is 1.1 Kg/s, calculate (i)the rate of condensation of steam (ii)the mean overall heat transfer co-efficient based on inner surface area (iii)the no. of transfer units (iv)the effectiveness of the condenser.
- Q.2** (a) What is baffle plate? Explain the importance and types of baffles with sketch. **07**
 (b) A double pipe heat exchanger is employed to heat raw water ($\dot{m}_c = 5 \text{ kg/s}$) from 15°C to **07**
 65°C using waste hot water ($\dot{m}_h = 4.83 \text{ Kg/s}$) cooled in the process from 95 to 75°C. The hot water flows in the inner tube (ID = 40mm, OD = 50mm) with 32 nos of longitudinal carbon steel fins (Fin Width = 0.89mm, Fin Height = 12.7mm & Root Width $W_r = 4.02 \text{ mm}$) in counter flow to the raw water which flows in annulus (ID = 75mm, OD = 90mm). Calculate the total length of heat exchanger. Consider $K_w = 60 \text{ W/m}^2 \text{ } ^\circ\text{K}$.
 OR
 (b) Using Kern method, Determine the overall heat transfer co-efficient for 2-P shell and **07**
 tube type heat exchanger for the given data: Shell internal diameter = 0.39m, Nos. of tubes = 124, Tube parameters –OD=19mm, ID = 16mm, $K_{\text{tube}} = 60 \text{ W/m}^2 \text{ } ^\circ\text{K}$, baffle spacing = 0.25m and cut = 25%, fouling resistance of $0.000176 \text{ m}^2 \text{ } ^\circ\text{K/W}$ on both side, Pitch size = 0.024m, $\mu_w = 6.04 \times 10^{-4} \text{ Ns/m}^2$. Mass flow rate = 13.88Kg/s
- Q.3** (a) Explain shell and tube type condenser. **07**
 (b) Determine the required face area of an R-12 condenser for 5 TR refrigeration plant. The **07**
 condensing temperature is 40°C, the system COP is 4.9 and refrigeration effect is 110.8 KJ/kg. Air at an inlet temperature of 27 °C flows through the condenser with a face velocity of 2.5 m/s. The inside and outside diameters of the tubes are 11.26 and 12.68 mm, respectively. Fin efficiency is 0.73. Vertical spacing in a tube in row = 43 mm; Tube spacing = 38 mm, centre to centre between fins = 3.175 mm, thickness of the fins = 0.254 mm. Nos. of rows = 4, Mean Reynolds No. = 431383, Condensation side $h_i = 8206.7 \text{ W/m}^2 \text{ } ^\circ\text{K}$. Use $\text{Nu}_o = 0.117 \text{ Re}^{0.65} \text{ Pr}^{0.33}$
 OR
Q.3 (a) Explain direct expansion type fin and tube evaporator. **07**
 (b) Write a short note on evaporative condenser. **07**
- Q.4** (a) What is a compact heat exchanger? Give the classification of compact heat exchanger. **07**
 (b) Air at 2 atm and 500 K with a velocity of 20 m/s flows across a compact heat exchanger **07**
 matrix having the configuration shown in fig 1(surface 11.32-0737-S-R). calculate the heat transfer coefficient and the frictional pressure drop. The length of the matrix is 0.8 m.
 OR
Q.4 (a) Write short note on fixed matrix type regenerator. **07**

- Q.4 (b)** A rotary regenerator, with a rotational speed of 10 rpm, is used to recover energy from a gas stream at 250°C flowing at 10 kg/s. This heat is transferred to the airstream at 10°C , also flowing at 10 kg/s. The wheel depth is 0.22 m and diameter 1.6 m, so that its face area is approximately 1.8 m^2 . The mass of the matrix is 150 kg with a surface-to-volume ratio of $3000 \text{ m}^2/\text{m}^3$, and the mean specific heat of the matrix material is $0.8 \text{ kJ/kg}\cdot\text{K}$. The heat transfer coefficient for both fluid streams is $30 \text{ W/m}^2\cdot\text{K}$. The mean isobaric specific heat of the gas is $1.15 \text{ kJ/kg}\cdot\text{K}$ and that of air is $1.005 \text{ kJ/kg}\cdot\text{K}$. The flow split gas: air = 50%: 50%. For a counter-flow arrangement, calculate the following values: **07**
- The regenerator effectiveness
 - The rate of heat recovery and the outlet temperatures of air and gas
 - The rate of heat recovery and the outlet temperatures of air and gas if the rotational speed of the wheel is increased to 20 rpm
 - The rate of heat recovery and the outlet temperatures of air and gas if the rotational speed of the wheel is reduced to 5 rpm
- Q.5 (a)** List the factors affecting cooling tower performance. **07**
- (b)** Warm water from a condenser at a rate of 100 kg/s enters the wet cooling tower at 32°C and is cooled by a moist humid air at 1 atm, 22°C and 60 percent relative humidity and it leaves at 25°C , saturated condition. The cooled water at the basin is 23°C . determine **07**
- Mass flow rate of air
 - Volumetric flow rate of air
 - Mass flow rate of make up water
 - Volumetric flow rate of cooling tower water.
- OR
- Q.5 (a)** Write a short note on forced draft cooling tower **07**
- (b)** Explain the components of cooling tower **07**

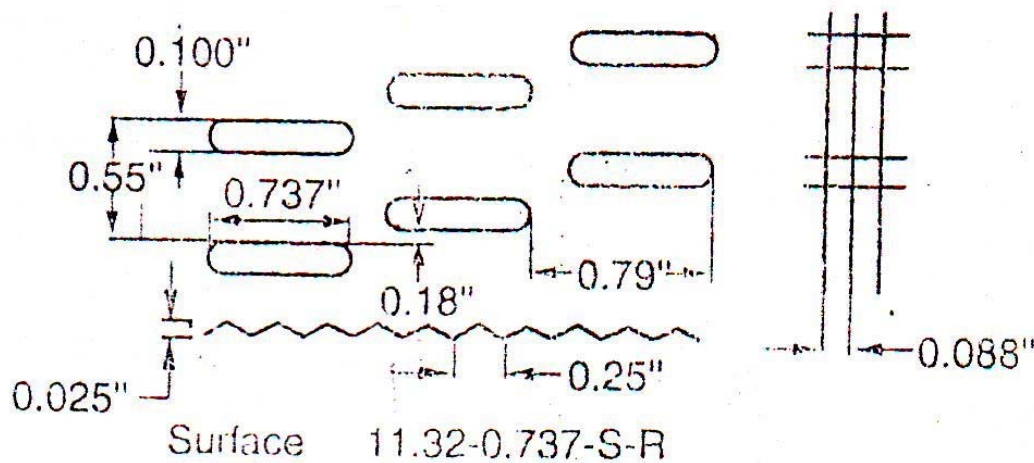


FIGURE 1

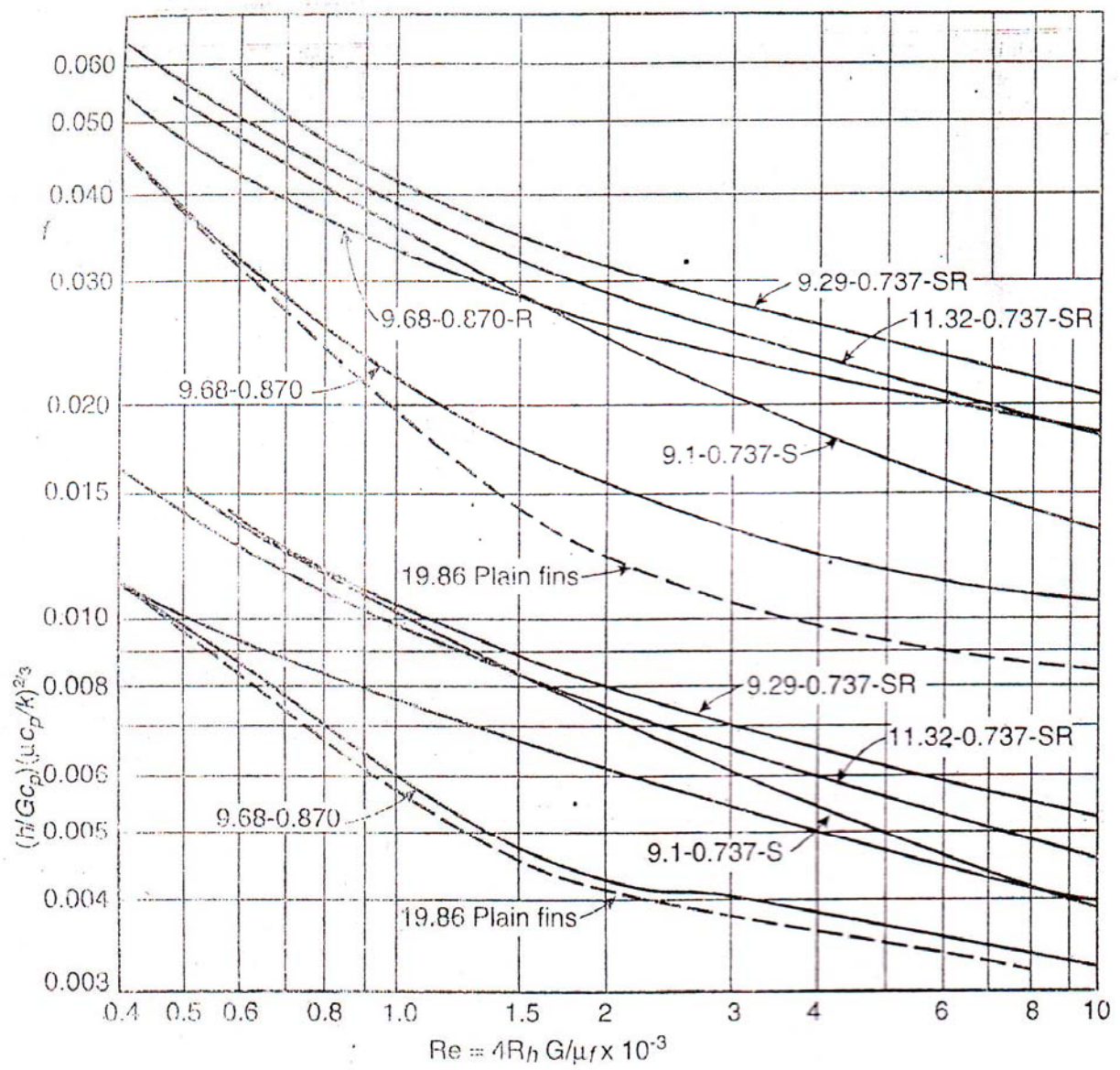


FIGURE 2
