

GUJARAT TECHNOLOGICAL UNIVERSITY**PDDC-Semester –VI (May-2012) Examination****Subject code: X61903****Subject Name: Heat and Mass Transfer****Date: 10/05/2012****Time: 10.30 am – 01.00 pm****Total Marks: 70****Instructions:**

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.
4. Use of properties tables permitted.

- Q.1** (a) Write the assumptions to be made as a base of Fourier's law of heat conduction. Also derive the equation for thermal conductivity of the body with the help of Fourier's law. **06**
- (b) Define the following laws. **08**
- i). Newton's law of cooling ii). Kirchhoff's law iii). Stefan-Boltzmann law
iv). Fick's law of diffusion

- Q.2** (a) Derive generalized heat conduction equation for non-homogeneous material without internal heat generation in Cartesian coordinates. **07**
- (b) A spherical container of negligible thickness holding hot fluid at 140°C and having an outer diameter of 0.4 m is insulated with three layers of each 50 mm thick insulation of conductivity of 0.02, 0.06 and 0.16 W/mK from inner to outer layers respectively. The outside surface temperature is 30°C . Calculate the heat loss and interface temperatures of insulating layers. **07**

OR

- (b) A spherical vessel of 0.05 m outside diameter is insulated with 0.2 m thickness of low temperature insulation of thermal conductivity 0.04 W/mK. The surface temperature of vessel is -195°C and outside air is at 10°C . Determine heat flow, heat flow per m^2 based on inside and outside areas and temperature gradients at the inner and outer surfaces. **07**
- Q.3** (a) State the purpose of thermal insulation. Also derive the equation for critical thickness of insulation for the sphere. **07**
- (b) Calculate the rate at which heat is being lost to the surrounding per unit length of an insulated steam pipe having the following dimensions and specifications. **07**
- $D_i = 3\text{ cm}$, $D_o = 3.4\text{ cm}$ for pipe, thickness of insulation = 1 cm, $h_i = 10\text{ W/m}^2\text{K}$ and $h_o = 10\text{ W/m}^2\text{K}$, $k_{(\text{pipe})} = 15\text{ W/mK}$ and $k_{(\text{insulation})} = 0.5\text{ W/mK}$, $t_{(\text{steam})} = 100^{\circ}\text{C}$ and $t_{\text{atm}} = 25^{\circ}\text{C}$.

OR

- Q.3** (a) Sketch the different fin configurations. Also write the assumptions are to be made for the analysis of heat flow through the fins. **07**
- (b) A longitudinal copper fin ($k = 380\text{ W/mK}$) 600 mm long and 5 mm diameter and insulated at tip is exposed to air stream at 20°C . The convective heat transfer **07**

coefficient is $20 \text{ W/m}^2\text{K}$. If the fin base temperature is 150°C , determine the heat transferred and the efficiency of the fin.

- Q.4** (a) Define the following terms **07**
 i). Boundary layer thickness ii). Nusselt number iii). Prandtl number
 (b) Explain with figure the various regimes of saturated pool boiling. **07**

OR

- Q.4** (a) Differentiate between the mechanism of filmwise and dropwise condensation. **07**
 (b) A vertical cylinder 1.5 m high and 180 mm in diameter is maintained at 100°C in an atmosphere environment of 20°C . Calculate heat loss by free convection from the surface of the cylinder. Assume properties of air at mean temperature as $\rho=1.06 \text{ kg/m}^3$, $\nu=18.97 \times 10^{-6} \text{ m}^2/\text{s}$, $C_p=1.004 \text{ kJ/kgK}$ and $k=0.042 \text{ W/mK}$. **07**

- Q.5** (a) Derive expression for logarithmic mean temperature difference for parallel heat exchanger. **07**
 (b) The overall temperature rise of the cold fluid in a cross flow heat exchanger is 20°C and overall temperature drop of hot fluid is 30°C . The effectiveness of heat exchanger is 0.60. The heat exchanger area is 1 m^2 and overall heat transfer co-efficient is $60 \text{ W/m}^2\text{K}$. Find out the rate of heat transfer. Assume both fluids are unmixed. **07**

OR

- Q.5** (a) Derive the equation $\frac{m_A}{A} = \frac{D}{L} (C_{A1} - C_{A2})$ of mass flux through the membrane with usual annotations. **07**
 (b) Determine the rate of heat loss by radiation from a steel tube of outside diameter 70 mm and 3 m long at a temperature of 227°C . if the tube is located within a square brick conduit of 0.3 m side and at 27°C . Take emissivity of steel and brick are 0.79 and 0.93 respectively. **07**
